

# Silica-Supported Cu Nanoparticle Catalysts for Alkyne Semihydrogenation: Effect of Ligands on Rates and Selectivity

Alexey Fedorov,\*<sup>®</sup> Hsueh-Ju Liu, Hung-Kun Lo, and Christophe Copéret

ETH Zürich, Department of Chemistry and Applied Biosciences, Vladimir-Prelog-Weg 1-5, CH-8093 Zürich, Switzerland

**Supporting Information** 

**ABSTRACT:** Narrowly dispersed, silica-supported Cu nanoparticles (ca. 2 nm) prepared via surface organometallic chemistry from a mesityl complex  $[Cu_5Mes_5]$  are highly active for the hydrogenation of a broad range of alkynes. Highthroughput experimentation allows for identifying the optimal ligand and reaction conditions to turn these supported Cu nanoparticles into highly chemo- and stereoselective catalysts for the preparation of *Z*-olefins (overall, 23 examples). For



instance, PCy<sub>3</sub>-modified Cu nanoparticles semihydrogenate 1-phenyl-1-propyne to *cis-\beta*-methylstyrene (20 bar H<sub>2</sub>, 40 °C) with turnover number and turnover frequency of ca. 540 and 1.9 min<sup>-1</sup>, respectively, and with 94% selectivity at full conversion.

### INTRODUCTION

Catalytic semihydrogenation of alkynes to alkenes is an important process in both industry and academia.<sup>1-7</sup> For instance, Pd catalysts are utilized for selective semihydrogenation of acetylene in ethylene feeds prior to ethylene polymerization.<sup>8</sup> Stereoselective semihydrogenation of internal alkynes to valuable Z-alkenes is a key step in the synthesis of vitamins and natural products.<sup>9,10</sup> Developed in the 1950s, the heterogeneous Lindlar catalyst (Pd/CaCO<sub>3</sub>/Pb(OAc)<sub>2</sub>/quinoline)<sup>11</sup> still remains a privileged system for Z-selective batch alkyne semihydrogenation.<sup>2-4,9</sup> However, it relies on expensive and rare palladium metal, uses toxic Pb additive, and has other limitations such as narrow substrate scope, overhydrogenation to alkanes, Z/E isomerization, and double bond migration reactions of olefin products. Commercial lead-free Pd-based catalysts with increased utilization of palladium were developed only very recently.<sup>12</sup> Approaches to improve the chemoselectivity of Lindlar-type catalysts relied on addition of ligands, for instance, organosulfides.<sup>13</sup> Semihydrogenation catalysts based on nanostructured Au<sup>14–19</sup> and Ag<sup>20–22</sup> were reported as well.

The scarcity and high price of noble metals has triggered the development of earth-abundant metal catalysts for alkyne semihydrogenation.<sup>23–26</sup> In particular, catalysts that utilize molecular Cu precursors and reductants such as hydrosilanes,<sup>27–29</sup> H<sub>3</sub>PO<sub>2</sub>,<sup>30</sup> or H<sub>2</sub><sup>31–33</sup> have recently emerged as an alternative to the Lindlar catalyst. However, these transformations often require high catalyst loadings (5–10 mol %) and H<sub>2</sub> pressures. That said, while supported Cu nanoparticles (NPs) are well-known active catalysts for propyne semi-hydrogenation in the flow settings,<sup>34–38</sup> the practical semi-hydrogenation of alkynes with Cu NPs in batch conditions remains underdeveloped.<sup>39</sup>

Here we describe the synthesis and characterization of narrowly dispersed, silica-supported Cu nanoparticles prepared

via surface organometallic chemistry (SOMC) approach.<sup>40</sup> These recyclable Cu NPs are highly active in alkyne hydrogenation at low loadings. The addition of various ligands to these Cu NPs, which is a general approach to modulate selectivity and activity of supported nanoparticle catalysts,<sup>41–45</sup> allows the improvement of the chemoselectivity of Cu alkyne semihydogenation catalyst. In particular, PCy<sub>3</sub>-modified Cu particles feature high turnover numbers and frequencies in a broad range of substrates.

### RESULTS AND DISCUSSION

Silica partially dehydroxylated at 700 °C (SiO<sub>2-700</sub>, 0.34 mmol  $\equiv$ SiOH g<sup>-1</sup>, 1.0  $\equiv$ SiOH sites per nm<sup>2</sup>, Figure 1a) reacts with a toluene solution of  $[Cu_5Mes_5]^{46,47}$  (0.95 equiv with respect to  $\equiv$ SiOH, Mes = mesityl) to give a yellow material Cu<sub>x</sub>Mes<sub>x-1</sub>/  $SiO_{2-700}$  (*x* = 2–5). The mass balance analysis shows recovery of 0.27 equiv of [Cu<sub>5</sub>Mes<sub>5</sub>] and infers 0.68 equiv of grafted  $[Cu_5Mes_5]$ . An NMR-scale grafting experiment in benzene- $d_6$ confirms this stoichiometry and also shows that the ratio of released Mes-H to reacted amount of [Cu<sub>5</sub>Mes<sub>5</sub>] is ca. 1.3. This is explained by the equilibrium between [Cu<sub>5</sub>Mes<sub>5</sub>] and  $[Cu_2Mes_2]$  in solution<sup>46</sup> and a concomitant grafting of both species. The IR spectrum of the grafted material shows a nearly complete disappearance of the isolated  $\equiv$ SiOH band at 3745  $cm^{-1}$  upon treatment with [ $Cu_5Mes_5$ ] in toluene and appearance of new C–H bands at 3036, 2937, 2880, and 1600  $\text{cm}^{-1}$  (Figure 1b). These observations infer grafting of [Cu<sub>5</sub>Mes<sub>5</sub>], in contrast to [Au<sub>5</sub>Mes<sub>5</sub>] that does not graft onto SiO<sub>2-700</sub> under the same reaction conditions.<sup>48</sup> Subsequent treatment of  $Cu_x Mes_{x-1}/SiO_{2-700}$  material under H<sub>2</sub> flow at 300 °C for 12 h gives a dark-brown Cu/SiO<sub>2-700</sub>. Synthesis of Cu/SiO<sub>2-700</sub> can be easily performed on gram scale. The H<sub>2</sub>

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**Figure 1.** Synthesis (a), IR spectra (b), representative HAADF STEM micrograph and the corresponding particle size distribution of Cu/ $SiO_{2-700}$  after slow oxidation in air at room temperature (c).

treatment regenerates surface silanols, while the C–H bands vanish (Figure 1b). Elemental analysis of Cu/SiO<sub>2-700</sub> reveals 5.5 wt % of Cu, corresponding to 3.5 Cu per  $\equiv$ SiOH site in the dehydroxylated support, and only trace amount of carbon and hydrogen. High-angle annular dark field scanning transmission microscopy (HAADF STEM) reveals formation of narrowly dispersed Cu nanoparticles with an average size of 1.9  $\pm$  0.3 nm, as determined after slow exposure to air (Figure 1c). Note that the size of Cu NPs prepared by other methods typically ranges from 5 to 15 nm.<sup>49</sup>

Exposure of Cu/SiO<sub>2-700</sub> to 12.7 mbar CO gives two strong bands in the IR spectrum at 2093 and 2057 cm<sup>-1</sup> (Figure S3). These bands disappear upon evacuation at room temperature, which is characteristic for CO adsorption on metallic copper nanoparticles.<sup>50</sup> H<sub>2</sub> chemisorption shows that amount of effective Cu surface (Cu<sub>active</sub>) in Cu/SiO<sub>2-700</sub> is 0.31 mmol  $g^{-1}$  (Figure S6).<sup>51</sup>

Activity of Cu/SiO<sub>2-700</sub> in semihydrogenation was tested with a set of 10 alkynes (1–10) at 60 °C in toluene under 50 bar H<sub>2</sub> for 24 h with 0.375 mol % Cu<sub>active</sub> catalyst loading (Figure 2, entry 1, and Table S1). Cu/SiO<sub>2-700</sub> semihydrogenates 4-nonyne (1) and 5-decyne (2) to Z-olefins with good chemo- and stereoselectivity and high conversion. Replacement of a longer alkyl group in 1–2 by a methyl group in 2-nonyne (3) deteriorates the Z-selectivity (Z/E ratio = 0.6). While the Z-content with 2,10-dodecadiyne is moderate, the conversion is low (4). Terminal 1-dodecyne (5) predominantly converts to dodecane instead of the olefin. Aryl alkyl and silyl alkynes (6–9) are overhydrogenated to alkanes under these reaction conditions. No reduction of aromatics (or solvent) was observed. Interestingly, the chemo- and stereoselectivity is greatly improved with electron-depleted ethyl phenylpropiolate (10). A possible explanation for this increase in selectivity is the lower reactivity of the thus-formed olefin or the poisoning of unselective Cu sites via the binding of the ester group.

A crucial component of the Lindlar catalyst is quinoline that poisons unselective Pd sites.<sup>11</sup> We therefore examined if addition of ligands can enhance the selectivity to Z-olefins. The ligands tested included phosphines (PPh<sub>3</sub>, (HO)PPh<sub>2</sub>, PCy<sub>3</sub>), a phosphine oxide PCy<sub>3</sub>(=O), an N-heterocyclic carbene (IMes = (1,3-bis(2,4,6-trimethylphenyl)imidazolidine), as well as *N*,*N*-dimethylaminopyridine (DMAP) (**L1-6**, Figure 2, entries 2–7). These ligands were added to H<sub>2</sub>-treated Cu/SiO<sub>2-700</sub> in ca. 5.3-fold excess with respect to the effective Cu surface area.

Overall, the addition of ligands resulted in significant improvement of chemo- and stereoselectivity to Z-olefins, albeit at the expense of mass activity (per Cu<sub>total</sub>) with some substrates. Compared to other ligands, phosphines yield higher Z-selectivity while maintaining high conversion of alkynes. Among phosphines tested, PCy<sub>3</sub> gives higher yields of Z-olefins. DMAP typically affords more alkanes, possibly due to the weaker binding to the Cu surface.  $PCy_3(=O)$  generally improves selectivity towards Z-alkenes with alkyl alkynes, but is not very effective with electron-rich aryl-substituted alkynes. Secondary phosphine oxide (HO)PPh2 and strongly donating and bulky IMes ligand are generally not efficient, but are selective with 1-phenyl-1-hexyne and 1-phenyl-1-propyne. Interestingly, PCy<sub>3</sub> and PCy<sub>3</sub>(=O) improve conversion of 10 compared to that of free Cu/SiO<sub>2-700</sub>. In contrast, the Lindlar catalyst overhydrogenates all alkynes to alkanes under the same reaction conditions.

Since PCy<sub>3</sub> performed best among ligands screened, yielding corresponding Z-alkenes with high selectivity due to reduced amounts of overhydrogenated and oligomerized products, Cy<sub>3</sub>P-Cu/SiO<sub>2-700</sub> was prepared by treating Cu/SiO<sub>2-700</sub> in pentane with 2.7-fold excess of PCy<sub>3</sub> per surface Cu<sub>active</sub>, followed by a removal of the unbound ligand by washing with pentane. By elemental analysis, Cy<sub>3</sub>P-Cu/SiO<sub>2-700</sub> contains 0.6 wt % P and ratios of C/P and H/P are ca. 21 and 26, respectively. This corresponds to 1.45 P per surface Cu atom. However, the IR spectrum of Cy<sub>3</sub>P-Cu/SiO<sub>2-700</sub> shows broadening of the silanol band indicating interaction of PCy<sub>2</sub> with  $\equiv$ SiOH (Figure S3). This suggests that silanols compete with the Cu surface for the phosphine binding, making the actual Cu nanoparticle coverage lower than inferred from the nominal loading. Based on the projected surface area of PCy<sub>3</sub>, ca. 70% of total  $Cu/SiO_{2-700}$  surface is covered by the ligand.

Cross-polarization (CP) magic angle spinning (MAS) <sup>31</sup>P NMR spectroscopy of Cy<sub>3</sub>P–Cu/SiO<sub>2-700</sub> reveals broad peaks at 33 and 27 ppm and a relatively sharp peak at 57 ppm (Figure S4c). The latter two peaks are also found in PCy<sub>3</sub> adsorbed on SiO<sub>2-700</sub> (Figure S4b) and are therefore attributed to the strongly adsorbed phosphonium species such as [ $\equiv$ SiO–H···· PCy<sub>3</sub>] or [ $\equiv$ SiO<sup>-</sup>···H–PCy<sub>3</sub><sup>+</sup>].<sup>52</sup> The peak at 33 ppm is likely due to interactions of PCy<sub>3</sub> with Cu NPs. Notably, addition of CO (34.6 mbar) gives rise to two CO adsorption bands at 2084 and 2007 cm<sup>-1</sup>, red-shifted compared to CO bands on Cu/ SiO<sub>2-700</sub> (Figure S3). Intensities of these bands are much lower

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#### conversion **Primary Ligand Screening** catalyst: Cu/SiO<sub>2-700</sub> or L-Cu/SiO<sub>2-700</sub> where L is: of alkyne selectivity to PPh<sub>3</sub> (HO)PPh<sub>2</sub> PCy<sub>3</sub> O=PCy<sub>3</sub> catalyst, 50 bar H<sub>2</sub> Z- or terminal L1 L2 L3 L4 4⊢ olefin (Eq. 1) toluene 60 °C 24 h increasing Othe values Products L5 L6 E-2H (CH<sub>2</sub>)<sub>4</sub> C<sub>6</sub>H<sub>13</sub> C<sub>10</sub>H<sub>21</sub> Pł C₄H<sub>9</sub> C₄H<sub>9</sub> Alkynes 1–10 Ĥ ċн Ρh т́мs COOF Ċ₂H₂ ċлна ċн ċн Ċ⊿H ĊН L 4\* entry none L1 L2 L3 L4 L5 L6 Comparison of Cu/SiO<sub>2-700</sub> (catalyst A) and Cy<sub>3</sub>P-Cu/SiO<sub>2-700</sub> (catalyst B) for alkynes 11-23 (eq. 1) \* Selectivity is (Z-2H + Z-2H,2H)



**Figure 2.** Top: identification of the optimal ligand for Cu/SiO<sub>2-700</sub>-catalyzed hydrogenation with a selected set of 10 alkynes; bottom: Cu/SiO<sub>2-700</sub> and Cy<sub>3</sub>P–Cu/SiO<sub>2-700</sub>-catalyzed alkyne hydrogenation with an additional set of 13 alkynes. See Table S1 for details. Conditions were as follows: substrate (400  $\mu$ mol), Cu/SiO<sub>2-700</sub> (5 mg, ca. 4.4  $\mu$ mol Cu total 1.5  $\mu$ mol Cu<sub>active</sub>), L1–L6 (8  $\mu$ mol) in 2 mL of toluene.

than those of unmodified Cu/SiO<sub>2-700</sub>, consistent with the decreased number of available surface sites, and the red shift of the CO band points to an increase of the electron density on Cu due to the PCy<sub>3</sub> binding. H<sub>2</sub> chemisorption shows that  $Cy_3P-Cu/SiO_{2-700}$  has an effective Cu surface area of 0.067 mmol g<sup>-1</sup> and a thermodynamic adsorption constant K = 3.44, corresponding to thermodynamic adsorption energy of -3 kJ mol<sup>-1</sup>, as opposed to the effective surface area of 0.14 mmol g<sup>-1</sup> and K = 948 for unmodified Cu/SiO<sub>2-700</sub> (Figure S6). This data supports a much weaker interaction of Cu surface with hydrogen in the case of PCy<sub>3</sub>-Cu/SiO<sub>2-700</sub>.

An additional set of alkynes (13 substrates), including more challenging terminal alkynes,<sup>53</sup> was then submitted to Cu/ $SiO_{2-700}$  and in situ prepared  $Cy_3P-Cu/SiO_{2-700}$  under the standard reaction conditions and the same total Cu loading (Figure 2, bottom). Whereas hydrogenation of phthalimidyl alkyne 11 proceeds with low conversion and high Z-selectivity, 2-butynyl benzoate 12 shows no conversion. Terminal alkynes 13–15 are readily hydrogenated, however, while PCy<sub>3</sub> does improve the selectivity to olefins, especially with 13; further optimization of pressure and temperature is necessary for these substrates. Higher reactivity of terminal alkynes compared to that of internal alkynes has been also observed for Pd/Al<sub>2</sub>O<sub>3</sub> catalysts.<sup>54</sup> While both catalysts oligomerize 16, switching to (HO)PPh<sub>2</sub> and IMes ligands, which proved generally inferior to PCy<sub>3</sub> in this study, allows for 88 and 70% selectivity to 16-Z-

2H, respectively (see Table S1). With exception of alkyne 18, the triple bond of activated diaryl-substituted alkynes 17-23 is semihydrogenated to Z-alkenes with Cy<sub>3</sub>P-Cu/SiO<sub>2-700</sub>. The nitro group in 18 is selectively reduced to the amino without reduction of the triple bond, although with a modest yield. In contrast, the acetyl group in 19 is reduced by both catalysts along with the triple bond; with PCy<sub>3</sub> ligand, the latter reduction is chemoselective to the olefin product. Pyridine moiety in 21 can presumably act as a ligand, making Cu/  $SiO_{2-700}$  catalyst more selective at the expense of activity. The C-Br bond in 22 is not reduced under the reaction conditions. The difficulty in the hydrogenation of alkynes with electrondeficient aryl substituent by Cu/SiO<sub>2-700</sub> is similar to what is observed with the Lindlar catalyst but is in contrast to goldbased catalysts.<sup>17</sup> With diyne 23, Cy<sub>3</sub>P–Cu/SiO<sub>2-700</sub> selectively yields Z-reduction of both triple bonds. Increasing the amounts of 6 and 8 by a factor of 4 results in similar conversions or selectivities with Cu/SiO<sub>2-700</sub> and Cy<sub>3</sub>P-Cu/SiO<sub>2-700</sub> (ca. 0.1 and 0.05 mol % Cu<sub>active</sub>, respectively) as those shown in Figure

To identify primary and secondary reaction products, we studied the progress of hydrogenation of 1-phenyl-1-propyne (6) at 40 °C under isobaric conditions (20 bar H<sub>2</sub>) with Cu/SiO<sub>2-700</sub> and Cy<sub>3</sub>P-Cu/SiO<sub>2-700</sub> catalysts using 0.375 and 0.18 mol % Cu<sub>active</sub>, respectively (Figure 3, Table S2). Both catalysts show zero-order dependence on alkyne concentration indicat-

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**Figure 3.** Evolution of concentration with time for the hydrogenation of 1-phenyl-1-propyne with Cu/SiO<sub>2-700</sub> (0.375 mol %, top) and Cy<sub>3</sub>P-Cu/SiO<sub>2-700</sub> (0.18 mol %, bottom) with dotted lines added to guide an eye.

ing a strong alkyne adsorption onto the Cu surface.<sup>53</sup> The unmodified catalyst Cu/SiO<sub>2-700</sub> is selective to  $cis-\beta$ -methylstyrene (6-Z-2H) until at least 70% conversion (120 min) and produces phenylpropane with 98% selectivity after 240 min. This demonstrates that overhydrogenation to alkane is a secondary process,<sup>24</sup> which is also confirmed by an in situ IR spectroscopy (see Supporting Information for details). In contrast, Cy<sub>3</sub>P-Cu/SiO<sub>2-700</sub> provides 6-Z-2H with 94% selectivity at full conversion of 6. The rates of Z-selective semihydrogenation of 1-phenyl-1-propyne to 6-Z-2H for the unmodified and phosphine modified Cu catalysts are  $1.2 \times 10^{-3}$ and 7  $\times$  10<sup>-4</sup> M s<sup>-1</sup>, which corresponds to TOF values corrected for the number of active sites determined by H<sub>2</sub> chemisorption of 1.5 and 1.9 min<sup>-1</sup>, respectively. Since poisoning of the most active but unselective sites by added ligands typically decreases reaction rates of heterogeneous catalysts, this increase in TOF observed for Cy<sub>3</sub>P-Cu/SiO<sub>2-700</sub> compared to Cu/SiO<sub>2-700</sub> indicates a ligand-accelerated catalysis,<sup>55</sup> a highly desirable and actively researched phenomenon in heterogeneous systems.<sup>44,56–60</sup> The aforementioned IR data on CO binding to the phosphine-modified Cu NPs suggests an increase in electron density on the surface Cu atoms. This modification of electronic structure of the catalyst is due to the donation of electron density from PCy<sub>3</sub> to Cu. Coordination of the phosphine probably reduces the strength of alkyne binding, which may be a reason for the enhanced rate with  $Cy_3P-Cu/SiO_{2-700}$ .

To confirm the difference in reactivity of  $Cy_3P-Cu/SiO_{2-700}$  versus that of  $Cu/SiO_{2-700}$  in hydrogenation of *cis*-olefins, we subjected pure *cis-β*-methylstyrene to hydrogenation under reaction conditions presented in Figure 3. Whereas unmodified

Cu/SiO<sub>2-700</sub> fully converted ca. 270 equiv of 6-Z-2H to 6-4H after 2 h, Cy<sub>3</sub>P–Cu/SiO<sub>2-700</sub> was nearly inactive, converting only 3% of 6-Z-2H to 6-4H (Table S3). This data suggest that while the alkyne can displace the phosphine bound to Cu surface sites and thereby be hydrogenated to the Z-alkene the alkene is a too weak ligand for the Cu in the presence of phosphine.

We also examined if  $Cu/SiO_{2-700}$  and  $Cy_3P-Cu/SiO_{2-700}$ hydrogenate 1-phenyl-1-propyne at lower pressures and found that **6**-Z-2H forms already at 2 bar although conversion after 360 min dropped from 100 and 97% at 20 bar to 21 and 17% at 2 bar, respectively, and selectivity decreased yielding higher amount of oligomers (selectivities to **6**-Z-2H = ca. 65%, Table S2). Filtration tests were conducted as well and showed no further conversion of **6** after removal of Cu/SiO<sub>2-700</sub> or Cy<sub>3</sub>P– Cu/SiO<sub>2-700</sub> from the reaction mixture, demonstrating no leaching of copper in both cases. Finally, recycling experiments with diphenylacetylene show that the catalytic ability of Cy<sub>3</sub>P– Cu/SiO<sub>2-700</sub> is retained in the second run and gradually decreases to one-fourth after five cycles.

#### CONCLUSIONS

We reported that well-dispersed, silica-supported Cu NPs prepared in a highly controlled manner via surface organometallic chemistry are highly active for batch alkyne hydrogenation. The high-throughput ligand screening approach applied to a heterogeneous catalyst allowed identifying tricyclohexylphosphine as a potent ligand to increase the chemoselectivity of alkyne semihydrogenation. The optimal catalyst Cy<sub>3</sub>P-Cu/SiO<sub>2-700</sub> is thus an efficient, practical, sustainable, and cheap alternative to the Lindlar catalyst. Modification of the electronic structure of the catalyst surface by PCy<sub>3</sub> ligand is reflected in the red-shifted stretching frequencies of Cu-bound CO probe molecule. Such ligand effect not only improved the chemoselectivity but also gave a more active catalyst, indicating ligand-accelerated catalysis<sup>55</sup> and serving as a guide for further development of better catalytic systems.

#### ASSOCIATED CONTENT

#### Supporting Information

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Full experimental details and characterization data (PDF)

#### AUTHOR INFORMATION

#### **Corresponding Author**

\*E-mail: fedoroal@ethz.ch.

#### ORCID

Alexey Fedorov: 0000-0001-9814-6726

#### **Present Address**

H.-J.L.: Department of Applied Chemistry, National Chiao Tung University, 1001 University Road, Hsinchu, 30010, Taiwan.

#### **Author Contributions**

A.F. and H.-J.L. contributed equally to this work.

## Notes

The authors declare no competing financial interest.

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